

# **Modeling the chloride-induced corrosion initiation of steel rebar in concrete**

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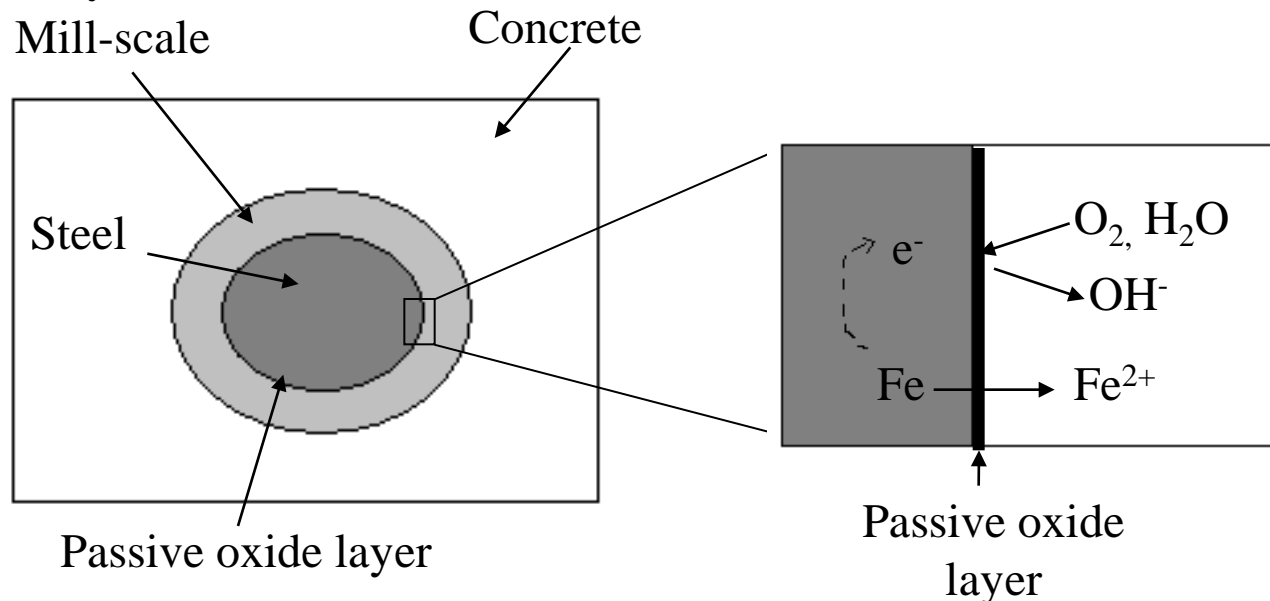
# Outline:

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- Introduction
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- Modeling: Domain and Boundary Conditions
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- Conclusion

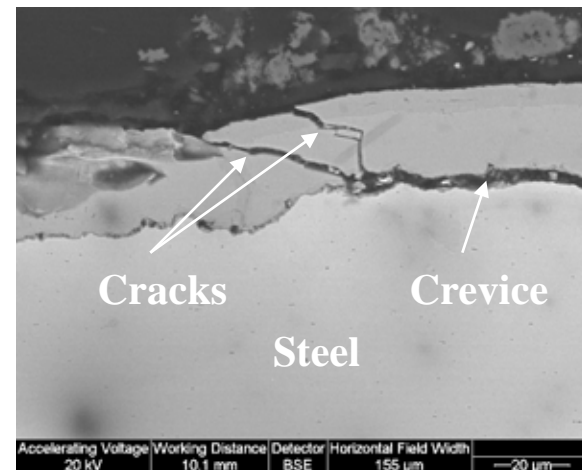
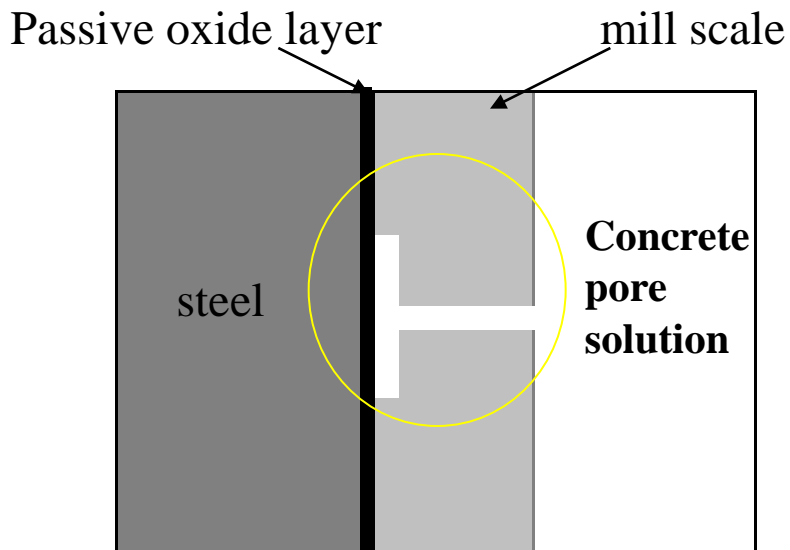
# Introduction:

- Generally-stable passive film formed on the steel surface under high alkaline conditions protects the steel against corrosion.
- Once passive film is destroyed (depassivation), corrosion will start.
- Mill-scale is an insoluble oxide layer that forms during steel production.
- It is approximately 50  $\mu\text{m}$  thick, crystalline in nature but poorly and non-uniformly attached to the rebar surface.



# Introduction:

- ❑ Corrosion preferentially initiates in the mill-scale crevices.
- ❑ Objective of this research is to explain the changes in chemistry of pore solution inside mill-scale crevices.
- ❑ Specifically to investigate the changes in the  $\text{Cl}^-/\text{OH}^-$ , which is an indicator of depassivation process.



# Modeling: Chemistry of Concrete Pore Solution

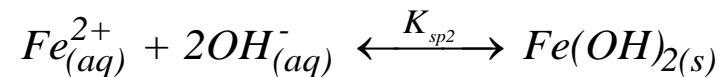
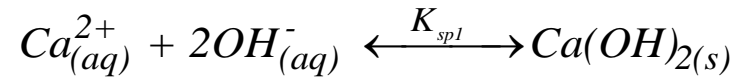
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- pH of concrete varies between 12.5 and 13.5.
- Solution 1 (pH=12.5): 9 species were considered in concrete pore solution:
  - $\text{OH}^-$ ,  $\text{OH}_{(s)}$ ,  $\text{Fe}^{2+}$ ,  $\text{Fe}_{(s)}$ ,  $\text{Ca}^{2+}$ ,  $\text{Ca}_{(s)}$ ,  $\text{Cl}^-$ ,  $\text{Na}^+$ ,  $\text{O}_2$
- Solution 2 (pH=13.5): 10 species were considered in concrete pore solution:
  - $\text{OH}^-$ ,  $\text{OH}_{(s)}$ ,  $\text{Fe}^{2+}$ ,  $\text{Fe}_{(s)}$ ,  $\text{Ca}^{2+}$ ,  $\text{Ca}_{(s)}$ ,  $\text{Cl}^-$ ,  $\text{Na}^+$ ,  $\text{K}^+$ ,  $\text{O}_2$

# Modeling: Chemistry of Concrete Pore Solution

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## □ Reversible chemical reactions:



## ■ Solubility relations:

$$\gamma_{Ca}[Ca^{2+}] \gamma_{OH}^2 [OH^{-}]^2 = K_{sp1}$$

$$\gamma_{Fe} [Fe^{2+}] \gamma_{OH}^2 [OH^{-}]^2 = K_{sp2}$$

## ■ $Ca(OH)_{2(s)}$ and $Fe(OH)_{2(s)}$ relation:

$$2\{[Fe](s) + [Ca](s)\} = [OH](s)$$

# Modeling: Transport of Ionic Species

## □ Nernst-Planck differential equation

$$\frac{\partial c_{is}}{\partial t} + \frac{\partial c_i}{\partial t} + \nabla \left( \underbrace{-D_i \nabla c_i}_{\text{Diffusion}} - \underbrace{\frac{D_i z_i F}{RT} c_i \nabla \phi}_{\text{Electrical Migration}} - \underbrace{D_i c_i \nabla (\ln \gamma_i)}_{\text{Chemical Activity}} \right) = 0$$

## □ Poisson's equation (electroneutrality)

$$\nabla^2 \phi + \frac{F}{\varepsilon} \sum_{i=1}^N z_i c_i = 0$$

$c_i$  = concentration of species in the ionic state (mol/m<sup>3</sup>)

$c_{is}$  = concentration of species in the solid state (mol/m<sup>3</sup>)

$\phi$  = potential gradient (V)

$\gamma_i$  = chemical activity coefficient

$D_i$  = diffusion coefficient (m<sup>2</sup>/s)

$z_i$  = valence of the species

$R$  = ideal gas constant (8.3143 J/mol/K)

$T$  = constant temperature (298K)

$F$  = Faraday's constant (96488 C/mol)

$\varepsilon$  = dielectric constant (7.092 x 10<sup>-10</sup> C<sup>2</sup>/N/m<sup>2</sup>)

# Modeling: Transport of Ionic Species

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- Modified Davies equation (Activity calculation)

$$\ln \gamma_i = -\frac{Az_i^2 \sqrt{I}}{1 + a_i B \sqrt{I}} + \frac{(0.2 - 4.17 \times 10^{-5} I) Az_i^2 I}{\sqrt{1000}}$$

where  $a_i$  is the radii of the ions, A and B are temperature dependent parameters, and I is the ionic strength of the solution

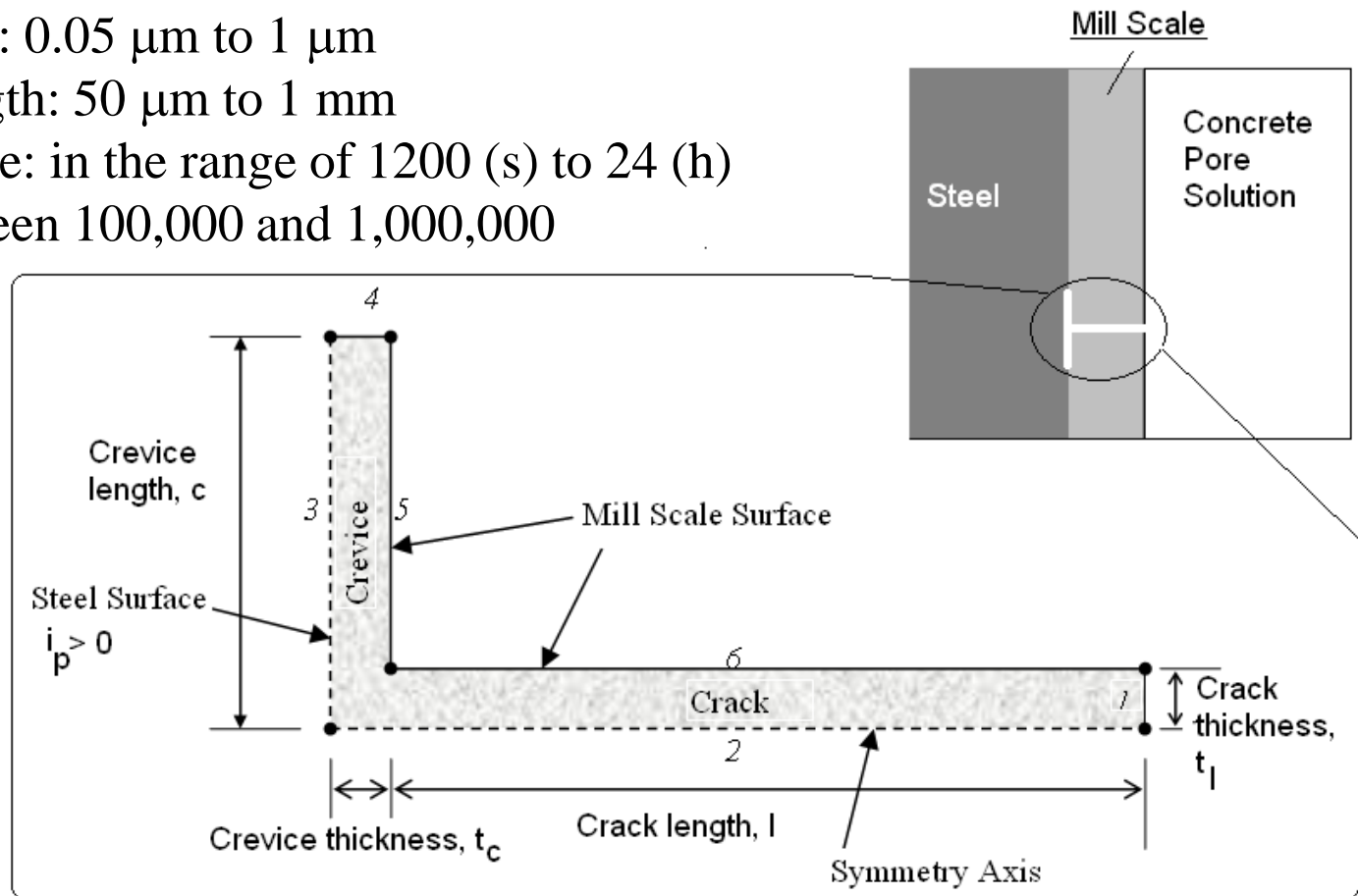
$$A = \frac{\sqrt{2} F^2 e_0}{8\pi (\epsilon RT)^{3/2}} \quad B = \sqrt{\frac{2F^2}{\epsilon RT}} \quad I = 0.5 \sum_{i=1}^N z_i^2 c_i$$

- Transient nonlinear finite element model was solved using COMSOL software



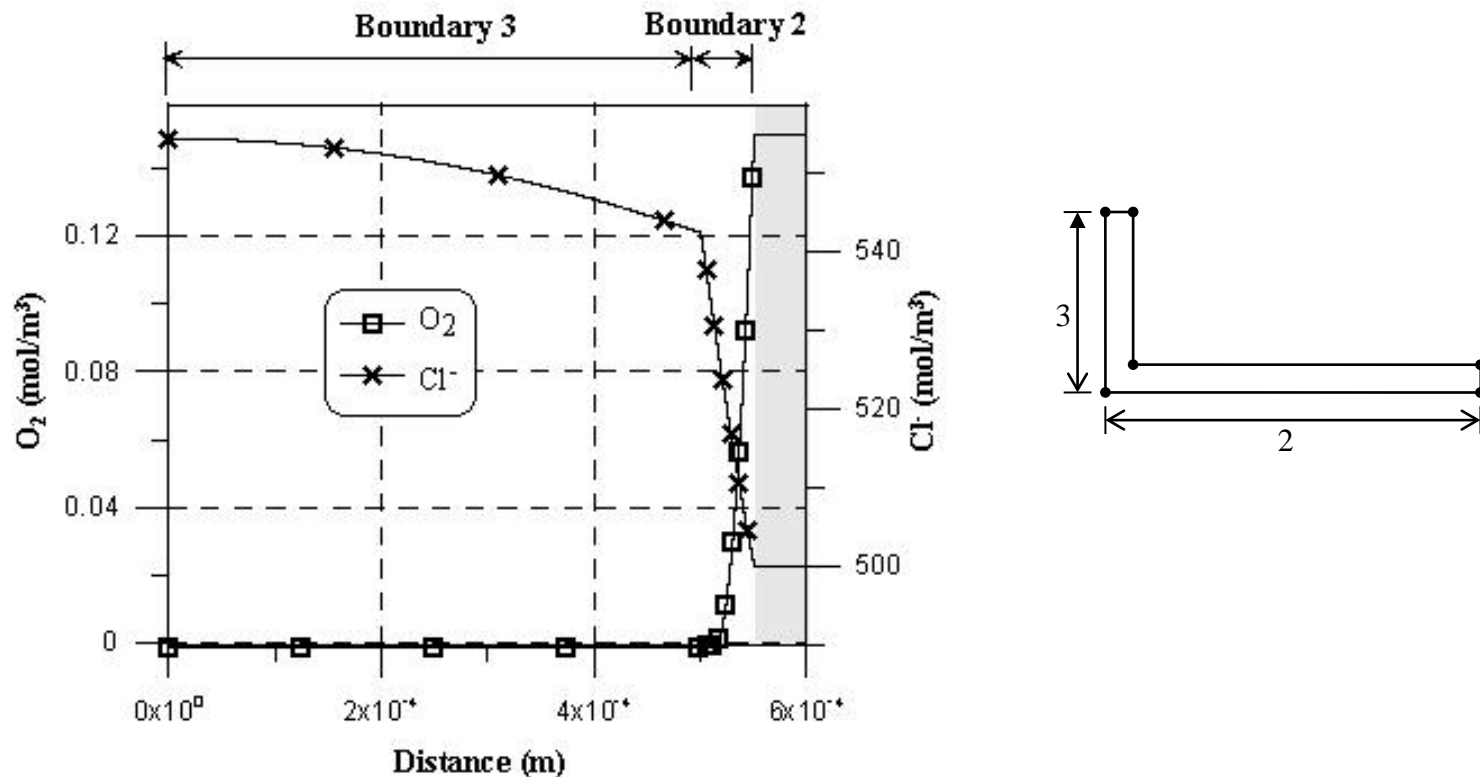
# Modeling: Domain and Boundary Conditions

- Crack width:  $0.05 \mu\text{m}$  to  $1 \mu\text{m}$
- Crevice length:  $50 \mu\text{m}$  to  $1 \text{mm}$
- Solution time: in the range of  $1200 \text{ (s)}$  to  $24 \text{ (h)}$
- DOF: between  $100,000$  and  $1,000,000$



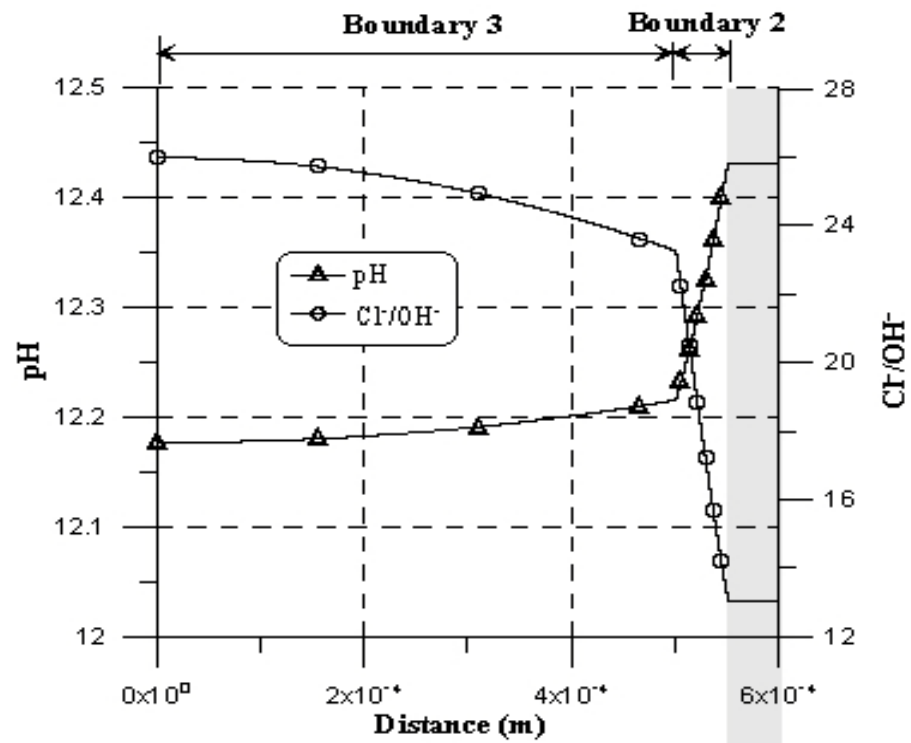
# Results – Oxygen, Chloride

- pH = 12.5, passive current density of 0.01 A/m<sup>2</sup>, 0.5 M chloride in bulk solution
- crack width = 0.1 μm, crevice length = 1 mm



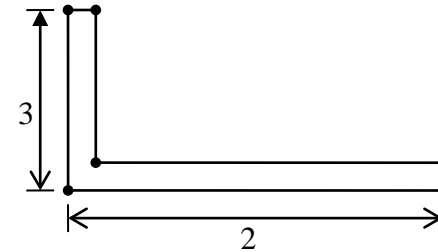
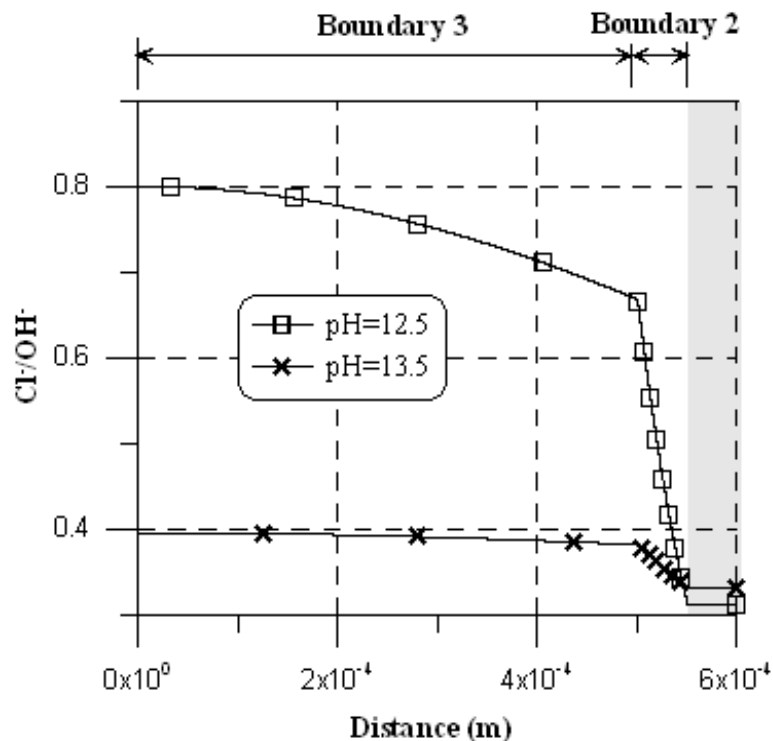
# Results - pH, Chloride-to-Hydroxide ratio

- pH = 12.5, passive current density of  $0.01 \text{ A/m}^2$ , 0.5 M chloride in bulk solution
- crack width =  $0.1 \text{ }\mu\text{m}$ , crevice length = 1 mm



# Results – Chloride-to-Hydroxide ratio

- $\text{Cl}^-/\text{OH}^-$  at different concrete pore solutions (pH = 12.5, pH=13.5)
- Passive current density of  $0.01 \text{ A/m}^2$ ,  $\text{Cl}^-/\text{OH}^- = 0.32$ , crack width =  $0.1 \mu\text{m}$ , crevice length = 1 mm



# Conclusions

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- The corrosion of rebar in concrete, a combination of electrochemical reaction and coupled ionic transport equation of several species, was successfully modeled using COMSOL(Ver. 3.5)
- The probability of corrosion initiation in the mill-scale crevices are higher:
  - Local acidification in crevice (reduction of  $\text{OH}^-$ )
  - Accumulation of chloride ions
  - Increasing chloride-to-hydroxide ratio ( $\text{Cl}^-/\text{OH}^-$ ), which is considered to be a key factor in corrosion initiation.

Thank You