



COMSOL
CONFERENCE
2016 MUNICH

Determination of Load Dependent Thermal Conductivity of Porous Adsorbents

O. Kraft¹, J. Gaiser¹, M. Stripf¹, U.Hesse²

¹University of Applied Sciences Karlsruhe

²TU Dresden



Hochschule Karlsruhe
Technik und Wirtschaft
UNIVERSITY OF APPLIED SCIENCES



GEFÖRDERT VOM

Bundesministerium
für Bildung
und Forschung



FORSCHUNG AN
FACHHOCHSCHULEN

Adsorption

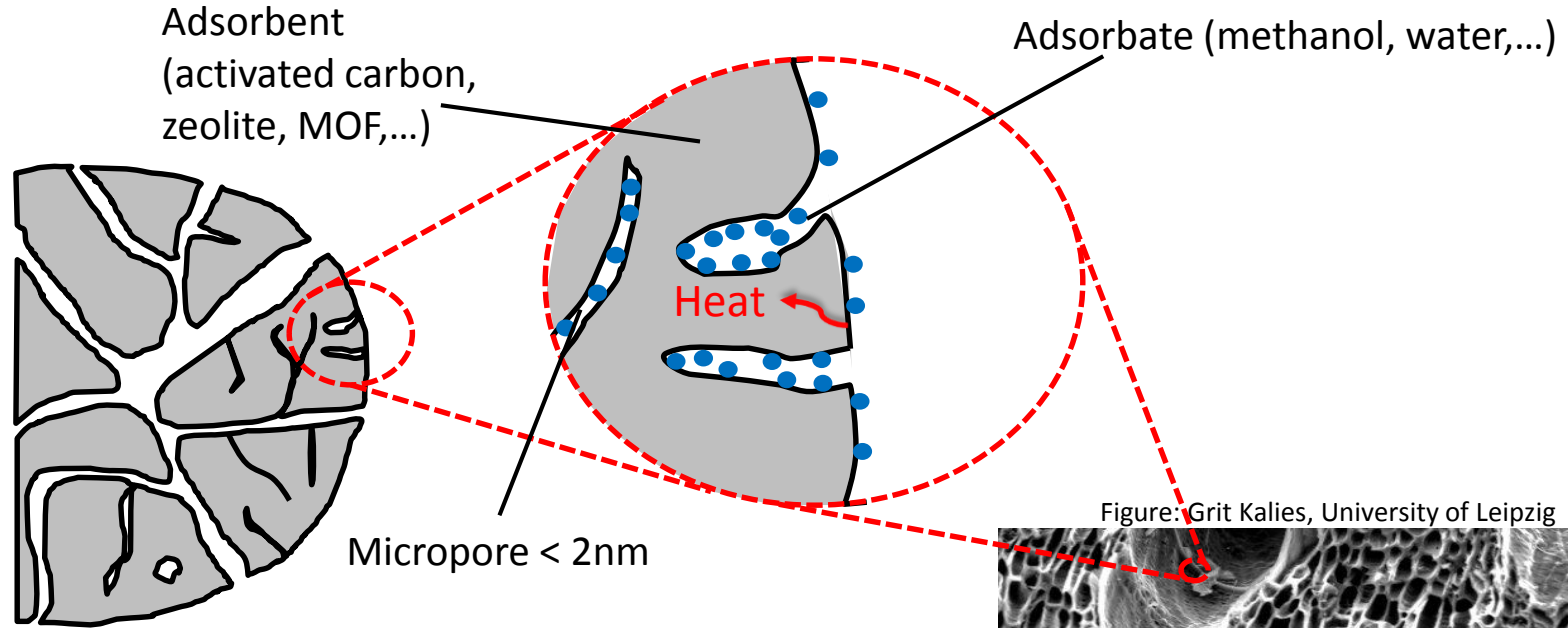
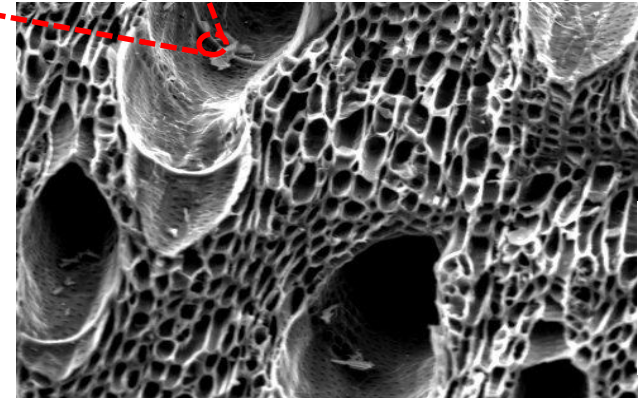


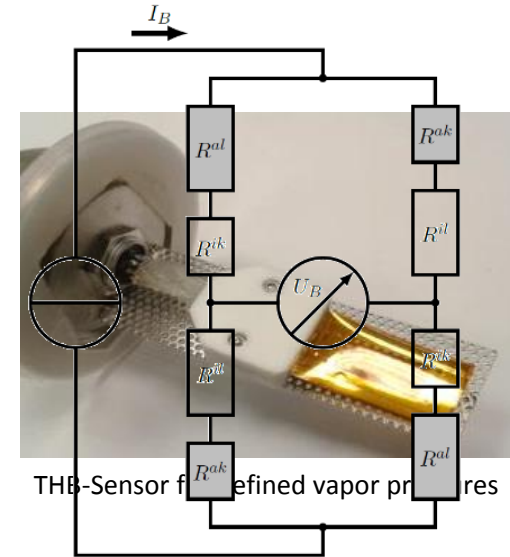
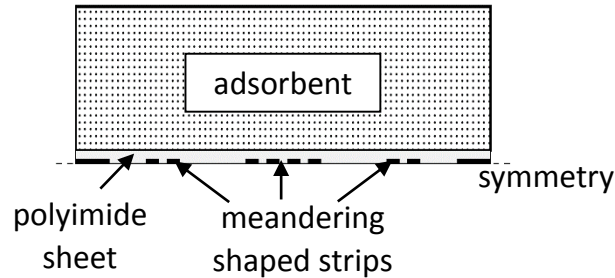
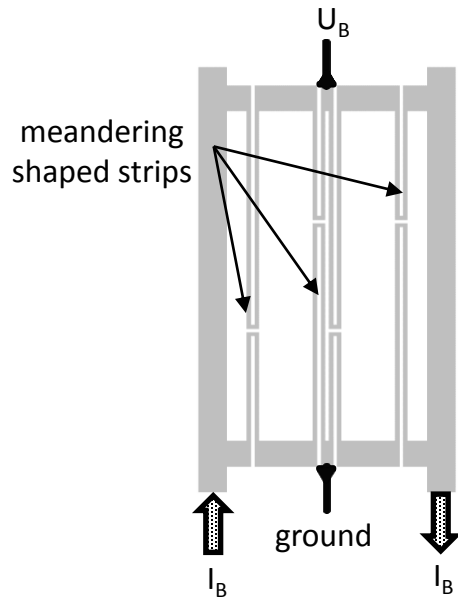
Figure: Grit Kalies, University of Leipzig



- Regenerative filters
- Purification of liquids and vapors
- Heat storage, Heat pumps

Principle of Transient Hot Bridge Technique

- Structured nickel film between two polyimid sheets
- Sensor clamped between two equivalent specimen

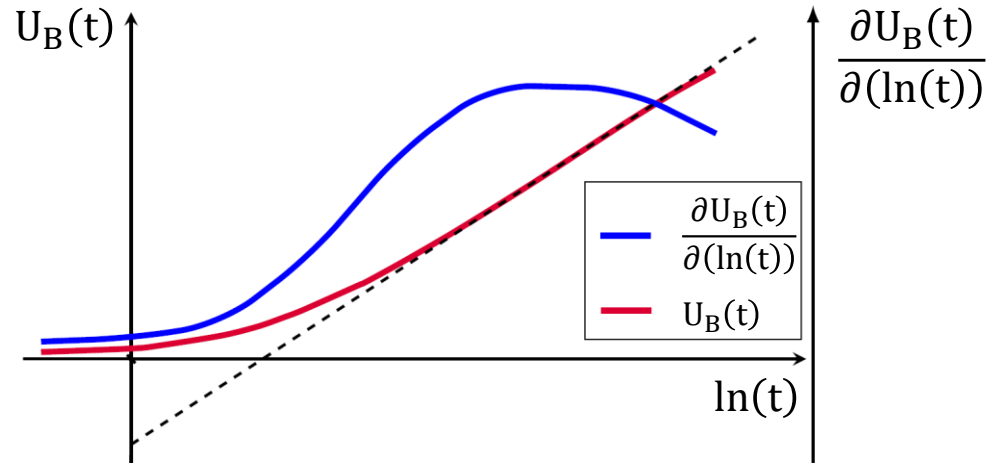


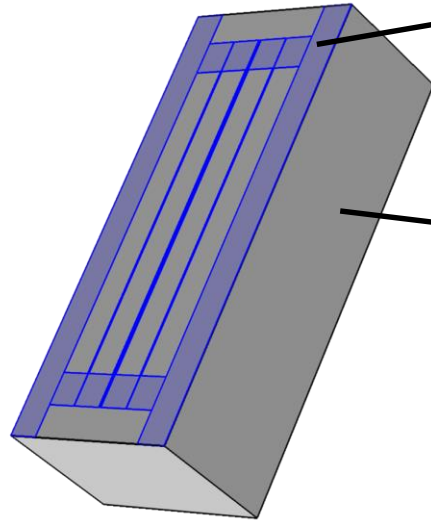
Wheatstone Bridge

Assumptions:

- Thickness of the sensor is negligible
- Sensor hot strips correspond to infinitely long flat heat sources
- Infinitely large samples with homogenous material properties

$$k_{\text{Specimen}} = \frac{\alpha R_0^2 I_B^3}{32\pi \left(\frac{\partial U_B(t)}{\partial(\ln(t))} \right)_{\max} L_s}$$





Geometry of sensor and specimen

Sensor-Physics:

- Heat Transfer in Solids
- Constant Current

Specimen-Physics:

- Heat Transfer in Porous Media
- Transport of Diluted Species in Porous Media
- Partial Differential Equation for Adsorption Process

Sensor

Heat Transfer in Solids

$$\frac{\partial T}{\partial t} = \frac{1}{\rho c_p} \cdot (\nabla(k\nabla T))$$

Constant Current

$$\nabla \left(-\sigma \nabla V + \frac{I_B}{d_{HS} \cdot b_{HS}} \right) = 0$$

Specimen

Transport of Dissolved
Species in Porous Media

$$\frac{\partial c}{\partial t} = \nabla(D\nabla c) - \frac{\rho_{Adb,dry}}{\epsilon \cdot M} \frac{\partial X_{ges}}{\partial t}$$

Partial Differential Equation
(Adsorption, multistage)

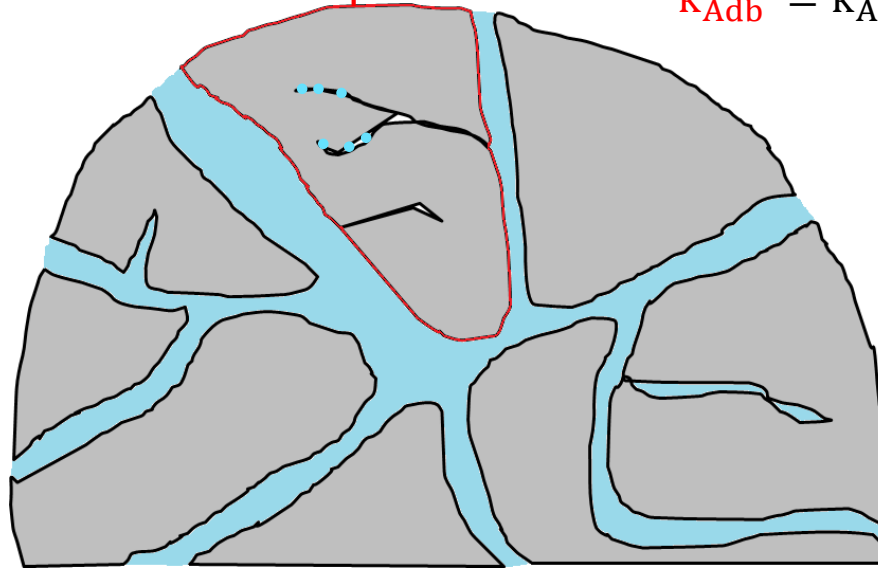
$$\frac{\partial X_{ges}}{\partial t} = \sum_{i=0}^n (\xi_i \cdot k_s A p_i \cdot (X_{GG} - X_i))$$

Heat Transfer
Porous Media

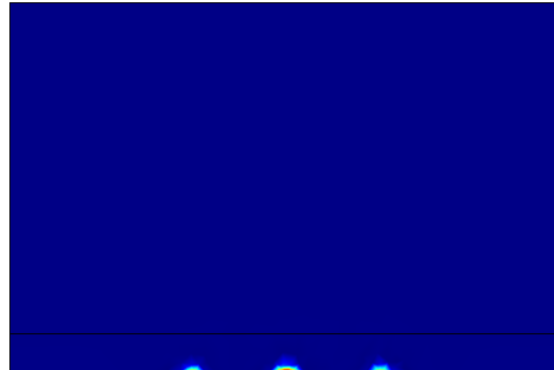
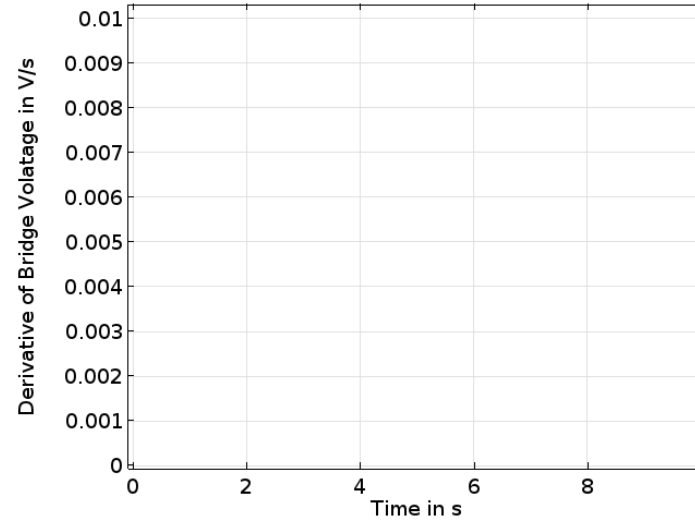
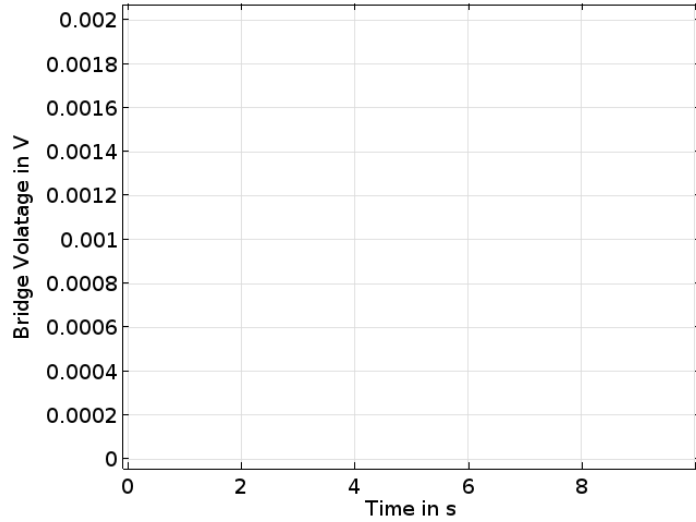
$$\frac{\partial T}{\partial t} = \frac{1}{(\rho c_p)_{\text{eff}}} \cdot \left(\nabla(k_{\text{eff}} \nabla T) + (\rho_v c_{p,v} \mathbf{u}) \nabla T + \frac{h_{\text{ad}}}{c_{p,\text{Adb}}(X_{\text{ges}}, T)} \frac{\partial X_{\text{ges}}}{\partial t} \right)$$

$$k_{\text{eff}} = \epsilon \cdot k_{\text{Adb}}(X_{\text{ges}}, T) + (1 - \epsilon) \cdot k_v(T)$$

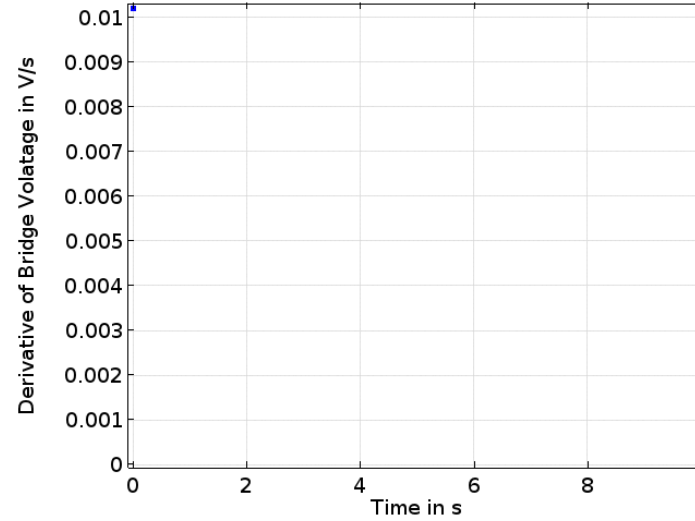
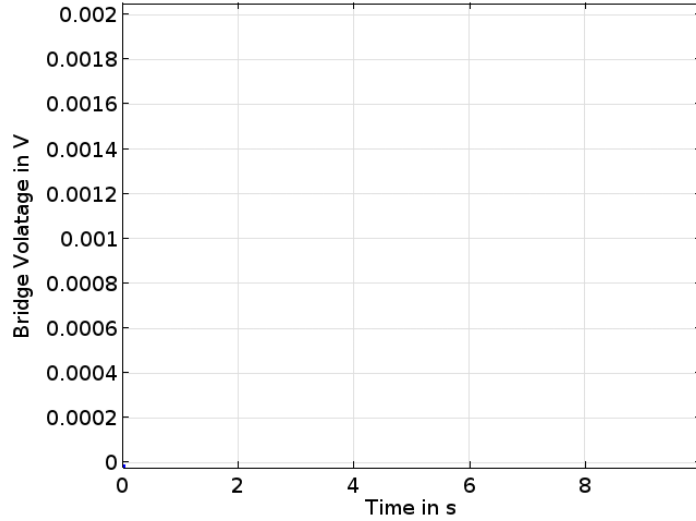
$$k_{\text{Adb}} = k_{\text{Adb,dry}} + f(X_{\text{ges}}, k_{\text{Fluid}})$$



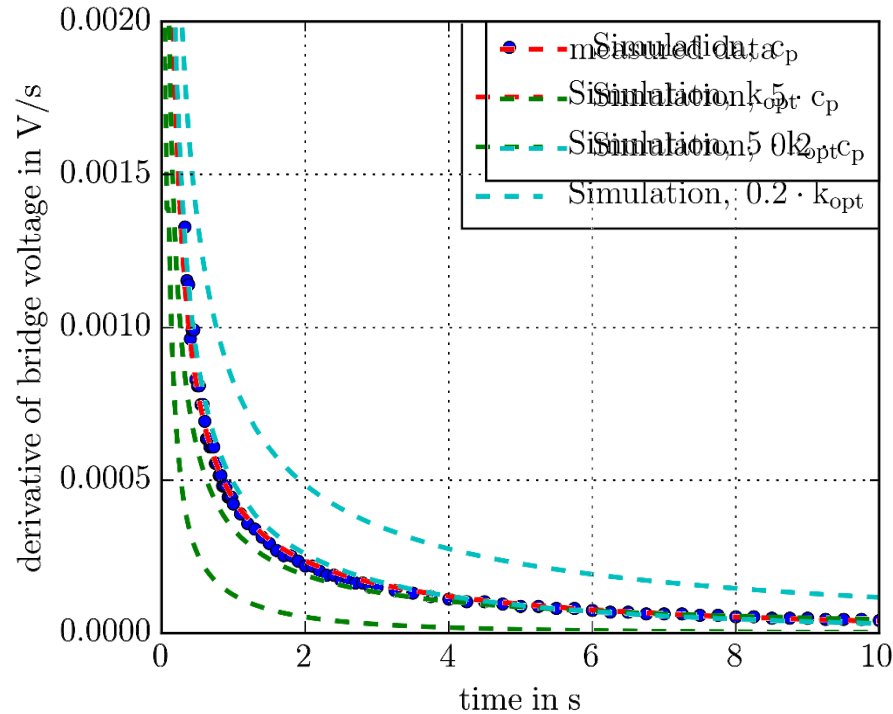
3D-COMSOL-Model



3D-COMSOL-Model

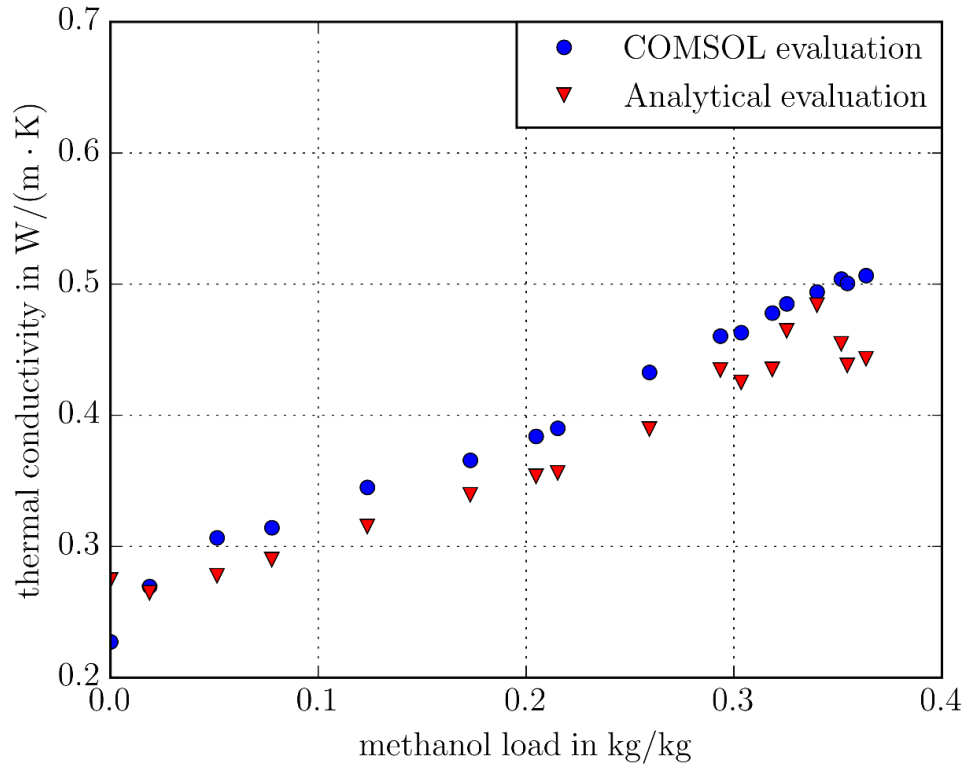


Use of Application Builder



- Automated evaluation of the load-dependent thermal conductivity
- Implementation of an optimization algorithm

Results

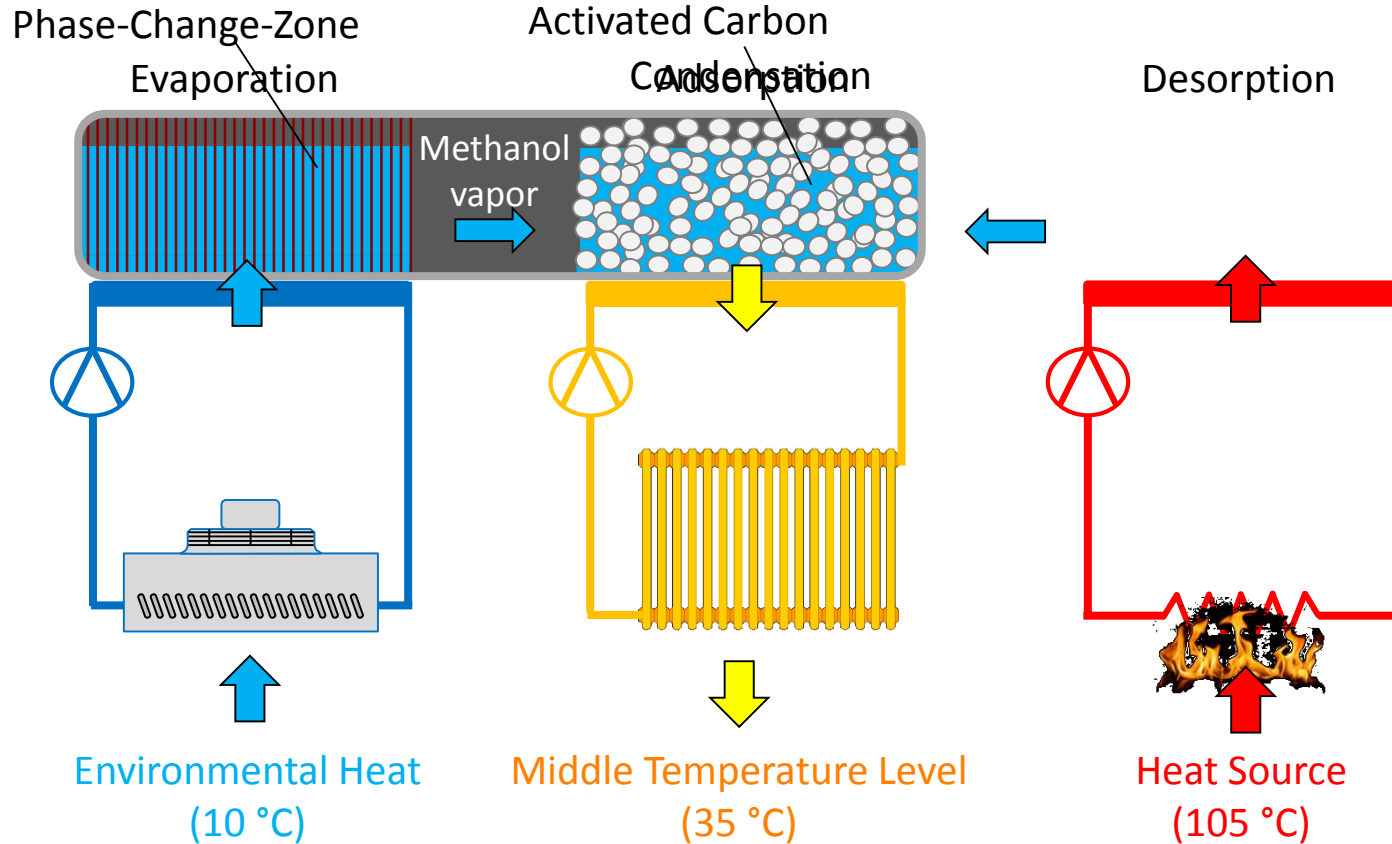


- No influence of the adsorption kinetics on the evaluation results
- COMSOL evaluation possible with low currents

- Determination of load dependent specific heat capacity
 - ➔ separation of solid and adsorbate heat capacity
- Determination heat capacity and thermal conductivity of specimen with
 - ➔ optimized heat transfer with high conductive additives

Backup

Principle of adsorption heat pump



Principle of adsorption heat pump

