



## Multi-Dimensional Adsorption Model of CO<sub>2</sub>/H<sub>2</sub>O Sorbent Bed

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COMSOL  
CONFERENCE  
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# Introduction



- The objective of this simulation effort is to develop and correlate a 2D axisymmetric adsorption model of the Vacuum Characterization test article in order to capture 3-D radial effect during adsorption.
- A 1-D baseline model has been created to understand the multi-physics being used during the adsorption process. However, this model only captures axial effects such as velocity, CO<sub>2</sub> concentration and temperature

# Approach

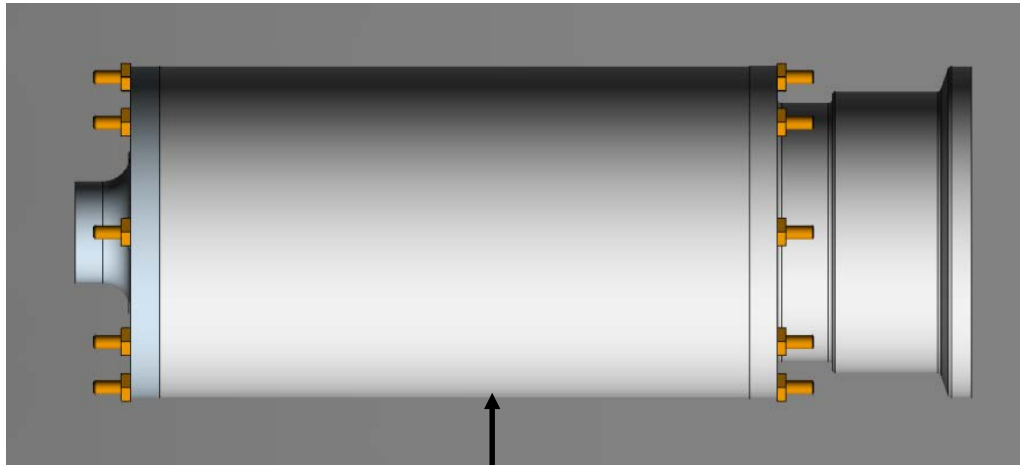


- The 2-D axisymmetric adsorption model has been developed to find and understand 3-D radial effects that a 1-D model cannot capture. Understanding these effects can help establish predictive capabilities that can be used to modify 1-D models for improved test correlations.
- This 2-D axisymmetric model includes COMSOL built-in Brinkman porous media flow interface which accounts for the fluid velocity and pressure fields in both the radial and axial direction.

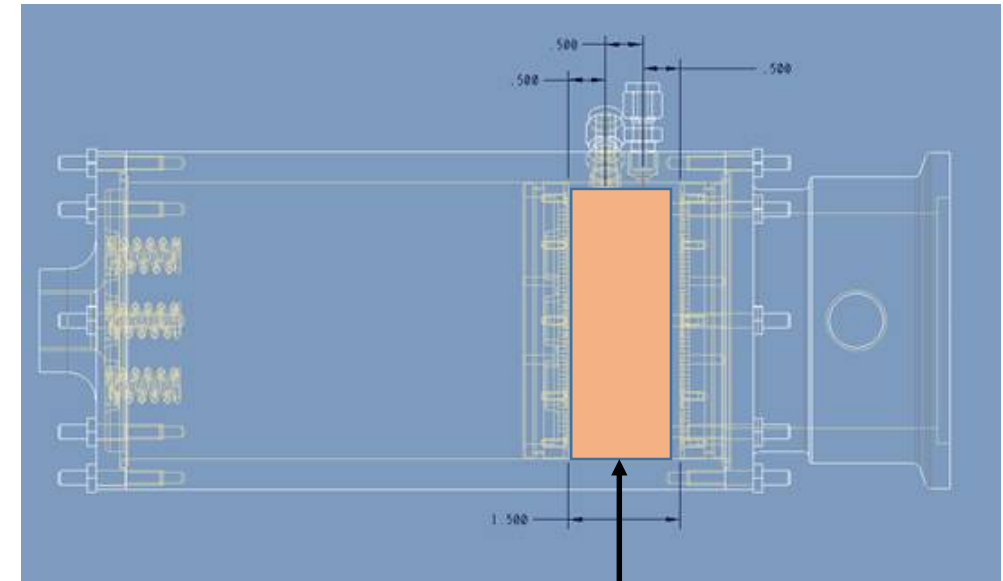
# Test Canister



- The canister contains a pelletized adsorption bed which is used to adsorb H<sub>2</sub>O and/or CO<sub>2</sub>.



6061 Aluminum canister with a 3.4" inner diameter

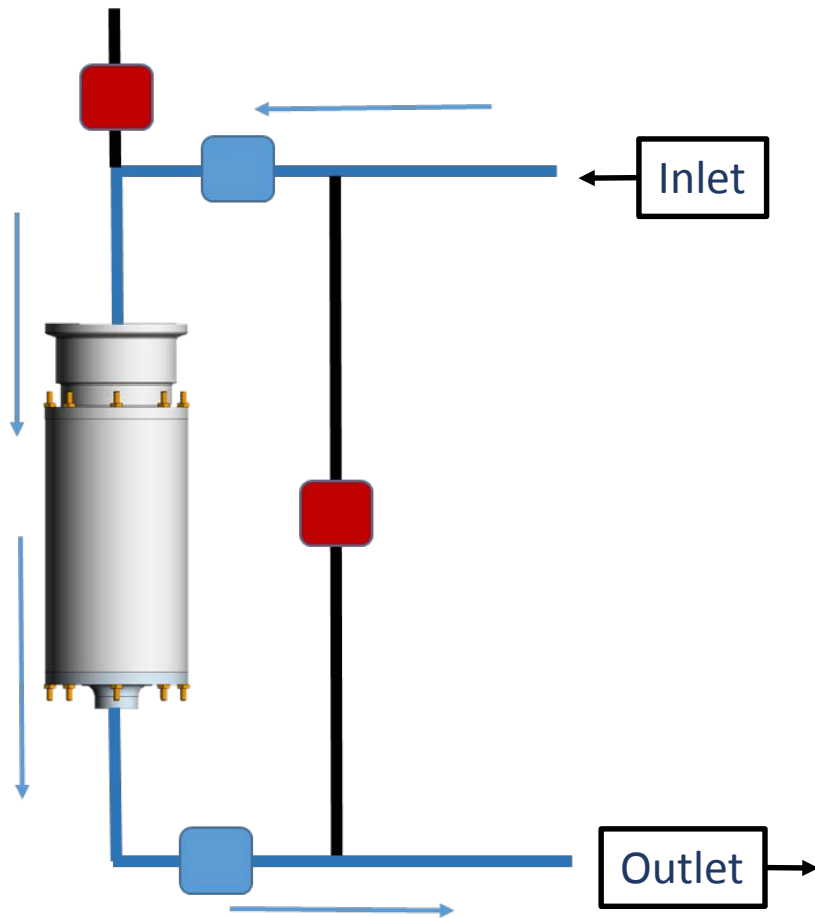


The bed length can be adjusted from 1" to 6"

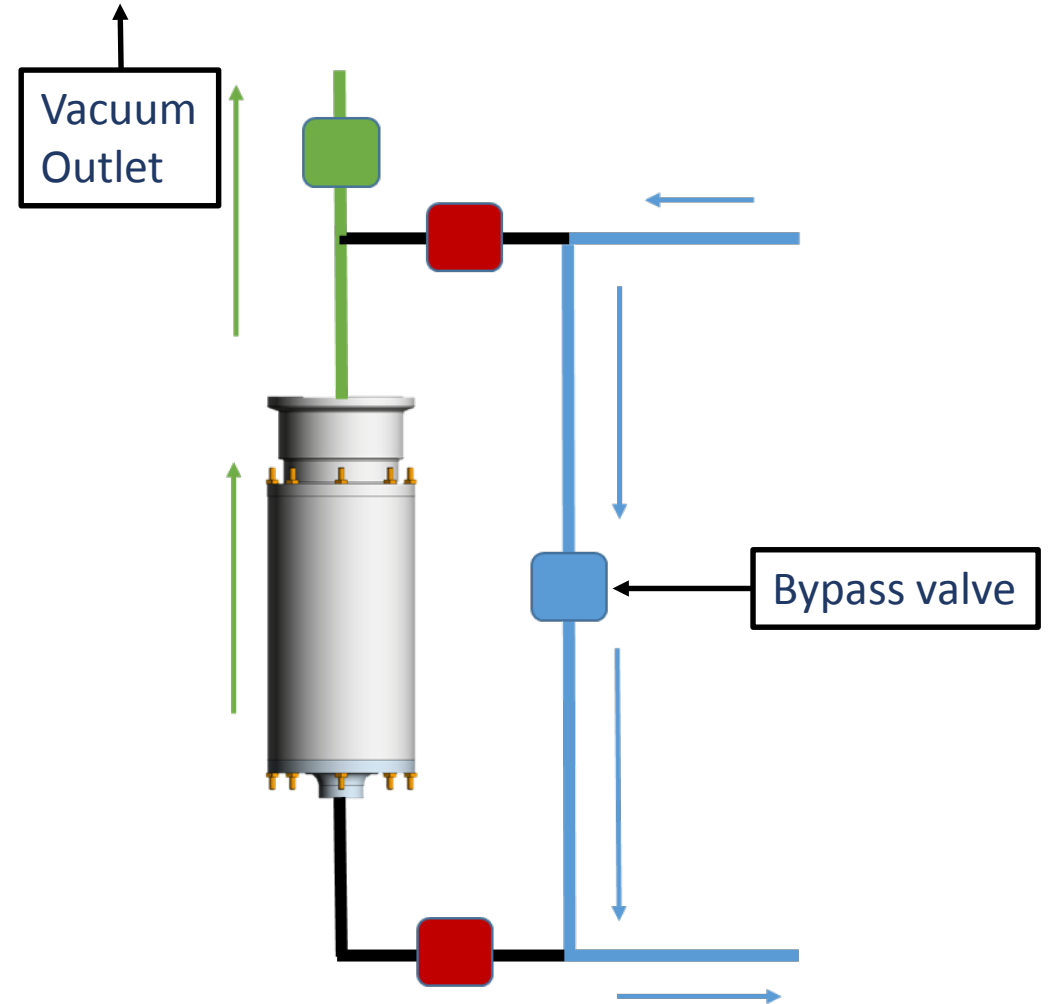
# Adsorption/Desorption Apparatus



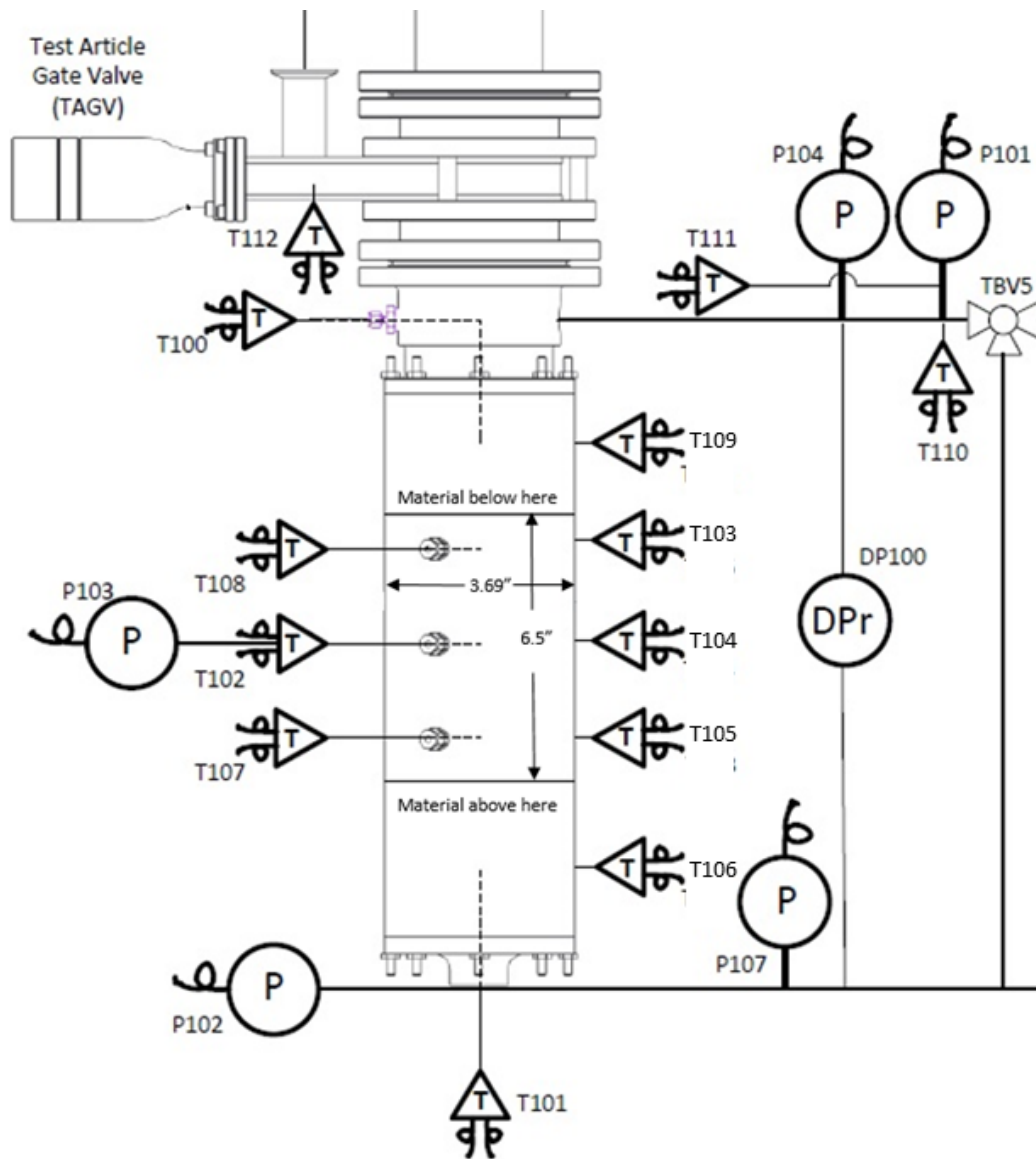
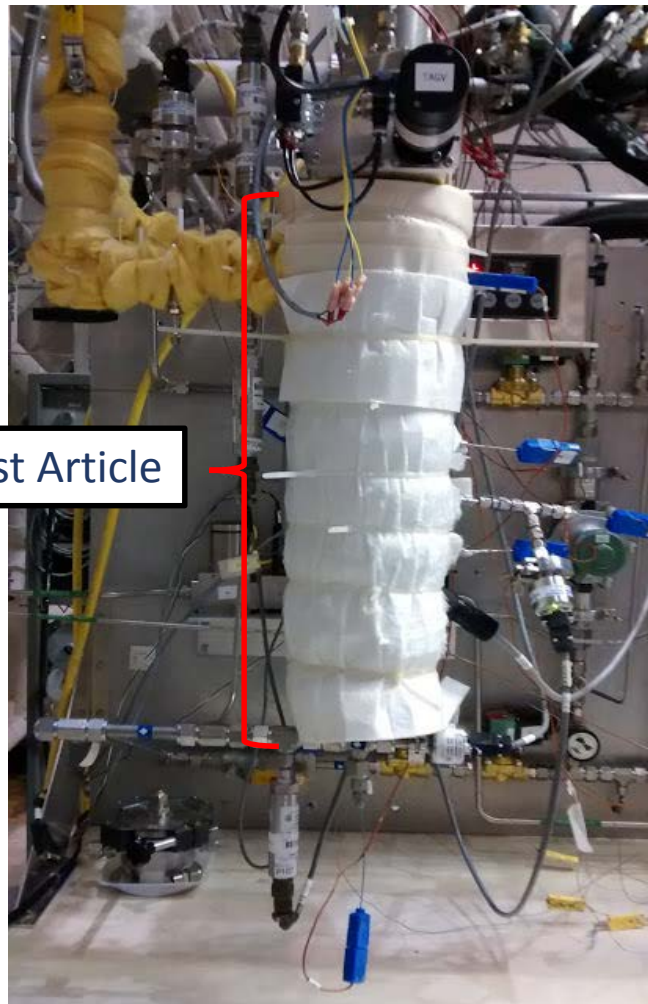
Adsorption flow direction



Vacuum desorption flow direction



# Test Article

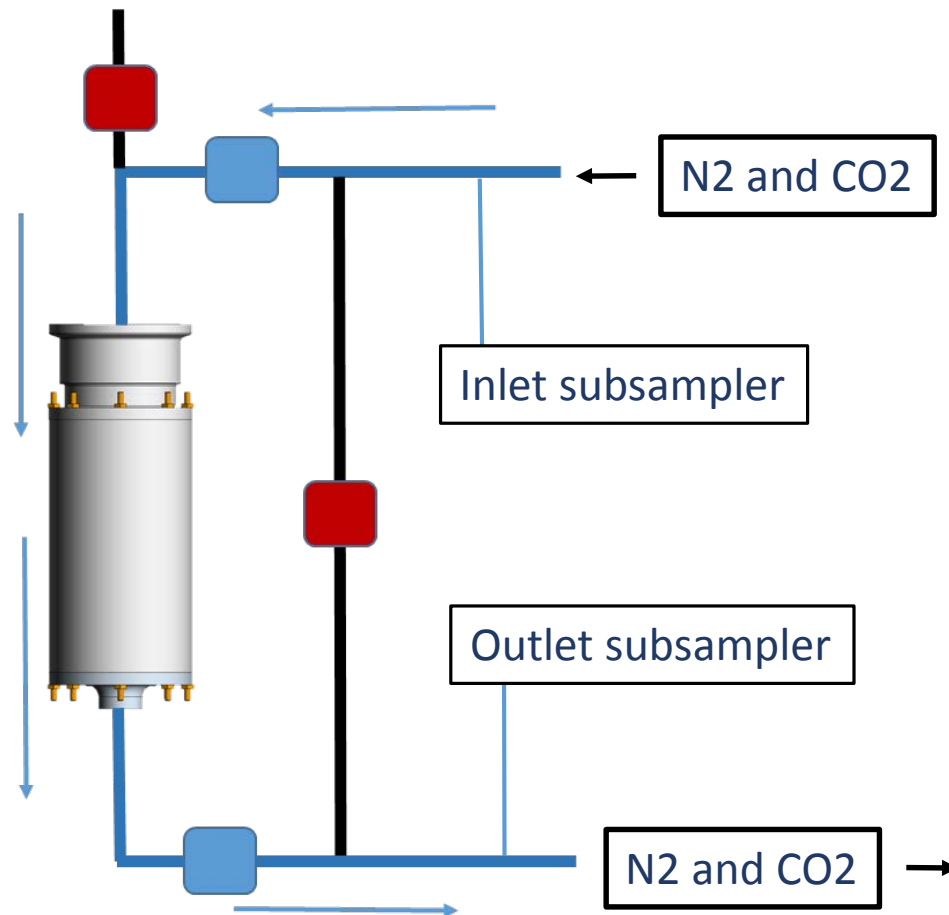


Photograph of test article covered in pyropropel (yellow) & fiberglass (white) insulation (taken 6-26-2015)

# Vacuum Characterization Breakthrough Test



Adsorption flow direction



- Nitrogen is used as a carrier gas in this experiment. Nitrogen and CO<sub>2</sub> are introduced at the inlet. The total flow is controlled by the Nitrogen flow controller
- Two CO<sub>2</sub> subsamplers are used to measure the influent and effluent CO<sub>2</sub> partial pressure
- The total mass flow, system pressures, CO<sub>2</sub> partial pressure, and inlet temperatures measurements are used as COMSOL model inputs.
- Internal and external temperature data are used to help correlate to the COMSOL model

# COMSOL Breakthrough Test Setup



Created a 2D axisymmetric model of the VC breakthrough test and compared results to test data

Model parameters:

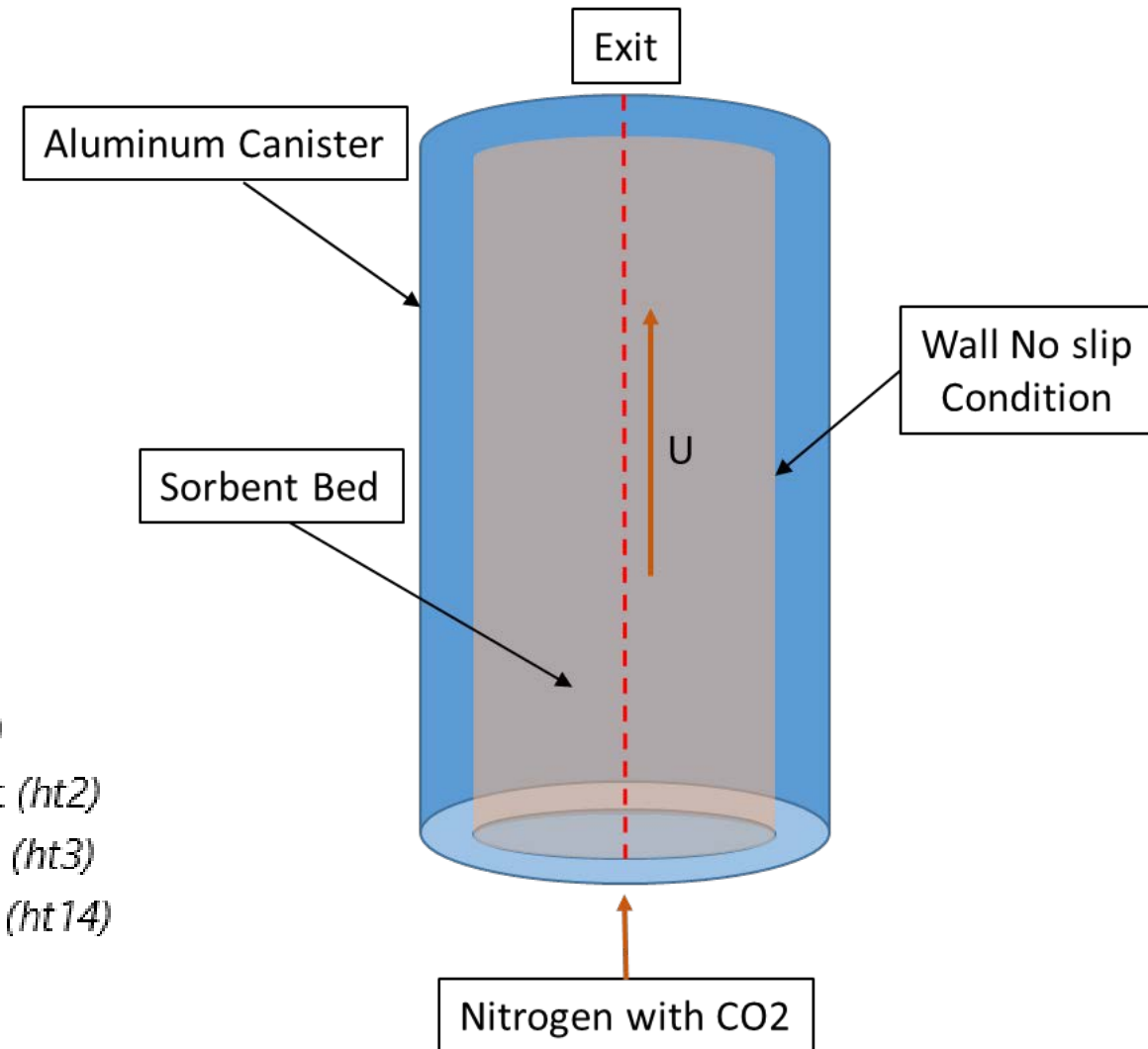
- 135 L/min
- Nitrogen and CO<sub>2</sub>
- 5A-RK38
- Constant Void Fraction/Variable Void Fraction

## 1D Modules

- ▶ Transport (S2) (*tcs3*)
- ▶ Heat Transfer in Can (*ht*)
- ▶ Heat Transfer in Sorbent (*ht2*)
- ▶ Heat Transfer in Fluid (*ht3*)
- ▶ Insulation (S2) (*ht14*)
- ▶ Darcy's Law (S2) (*dl4*)
- ▶  $\Delta u$  Loading (S2) (*q4*)

## 2D Modules

- ▶ Transport (S2) (*tcs3*)
- ▶ Heat Transfer in Can (*ht*)
- ▶ Heat Transfer in Sorbent (*ht2*)
- ▶ Heat Transfer in Fluids 3 (*ht3*)
- ▶ Heat Transfer Insulation (*ht14*)
- ▶  $\Delta u$  Loading (S2) (*q4*)
- ▶ Brinkman Equations (*br*)





# CO2 Loading PDE



Mass transfer rate represented in COMSOL

## Transport of Concentrated Species

Reaction: 
$$-\frac{\partial q}{\partial t} M_{CO_2} (1 - \varepsilon)$$

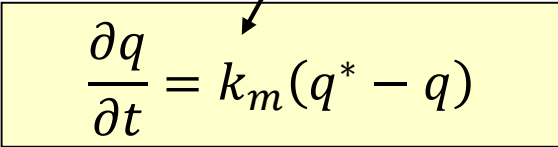
## Heat Transfer in Sorbent

Heat Source: 
$$-dh \frac{\partial q}{\partial t} (1 - \varepsilon)$$

## Brinkman Porous flow

Mass Source: 
$$-\frac{\partial q}{\partial t} M_{CO_2} (1 - \varepsilon)$$

Linear Driving  
force


$$\frac{\partial q}{\partial t} = k_m (q^* - q)$$

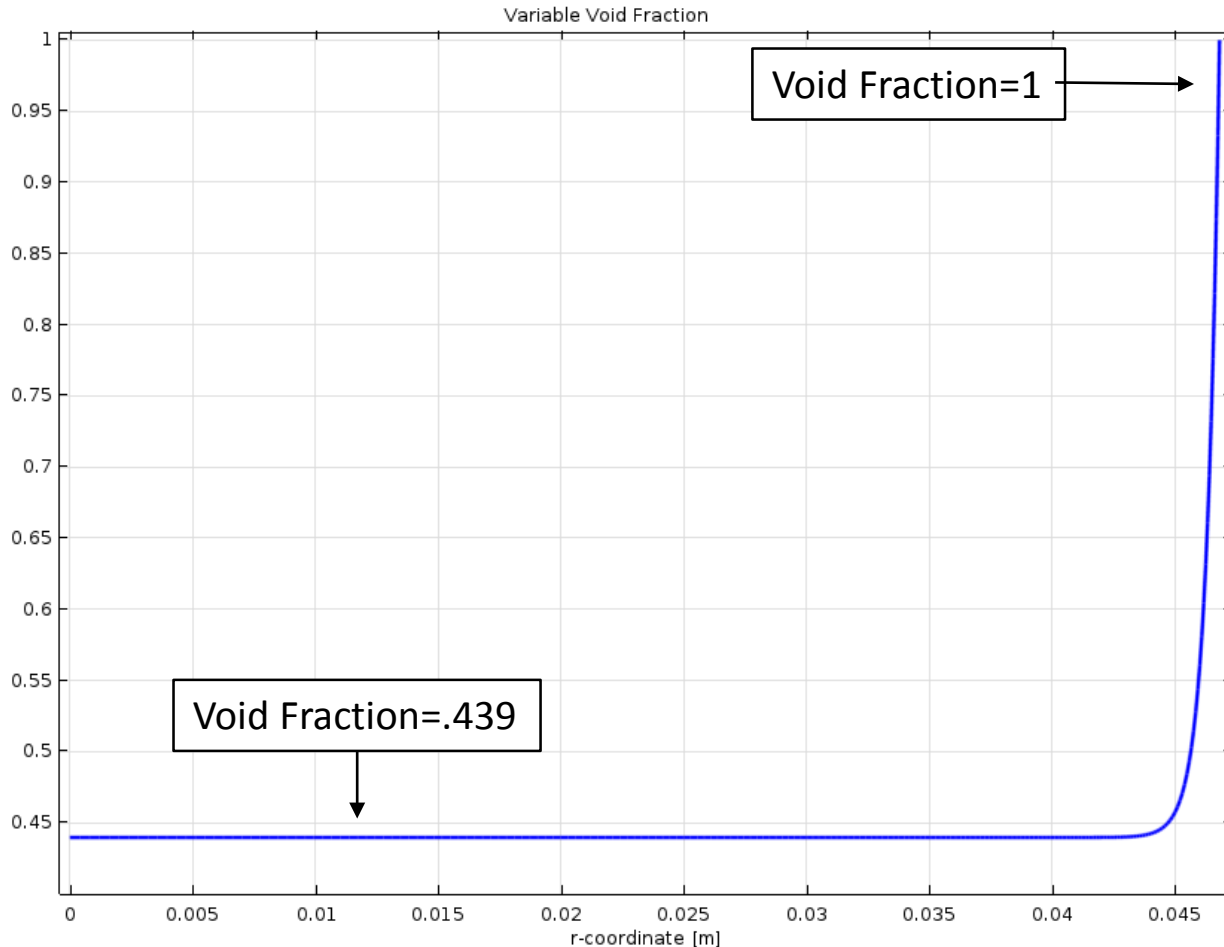
Governing Equation PDE

# Variable Void Fraction



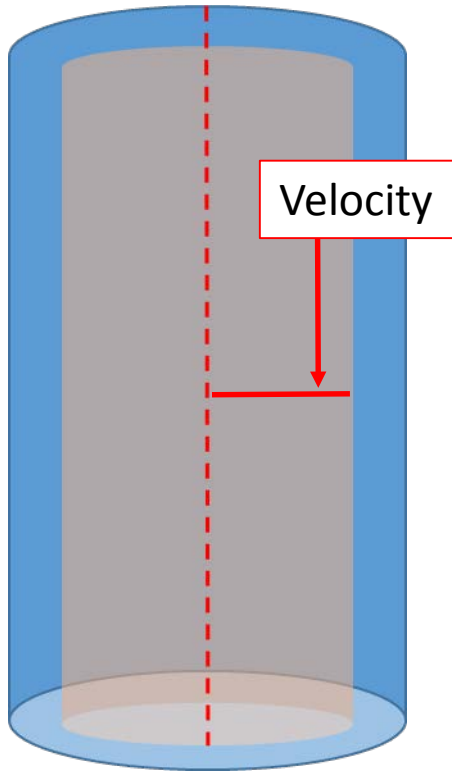
$$\text{Eps}_p = \text{VoidFraction} * (1 + C * \exp(-N * \max(0. [\text{m}], (\text{ColRad} - r)) / \text{EqPelDia}))$$

Tobias and Vortmeyer

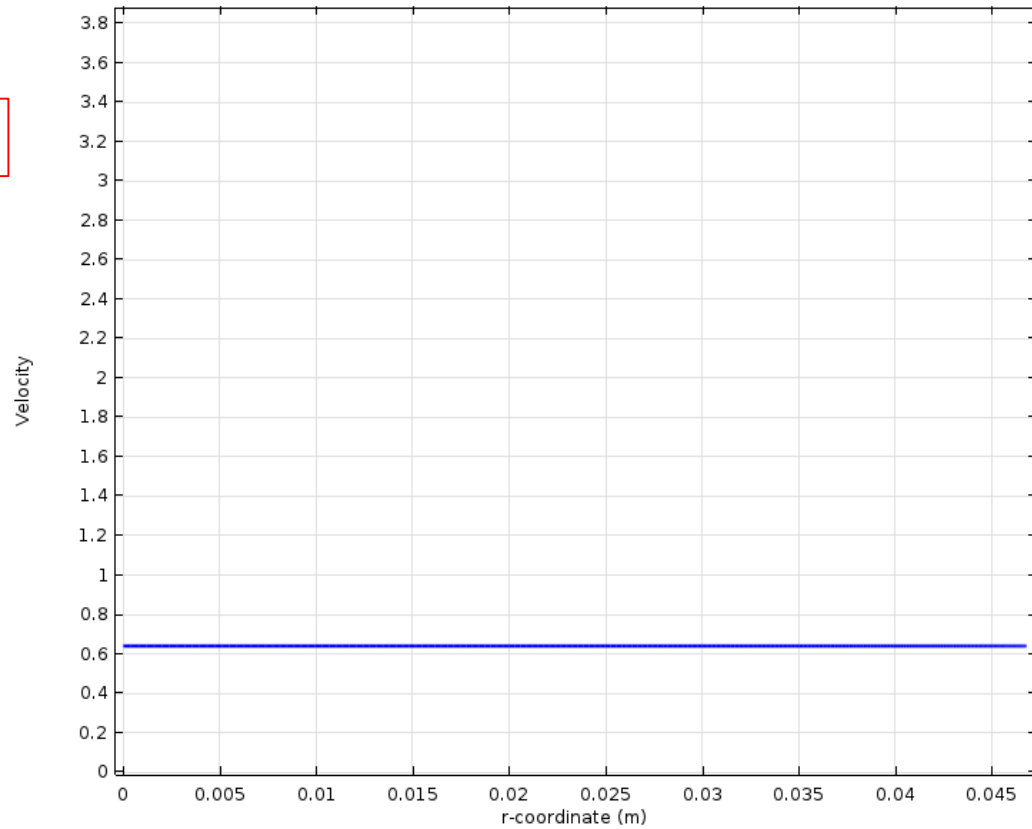


- The porosity varies sharply near the wall for a spherical packed bed since the geometry of packing is interrupted there. As a result, the velocity profile inside the packed bed is severely distorted near the wall.
- This phenomenon is known as flow channeling. A channeling effect was added to the model by using an expression that varies the porosity and increases it exponentially as it reaches the wall.

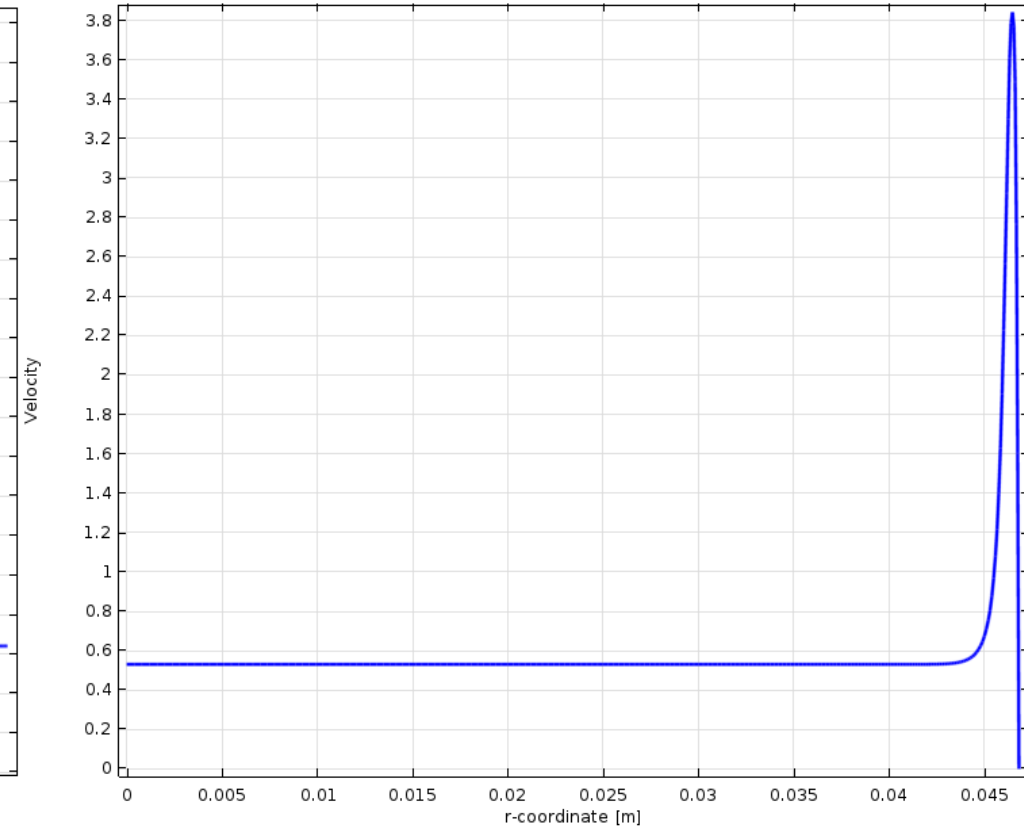
# Kappa Variable Void Fraction



### 2D Darcy Velocity



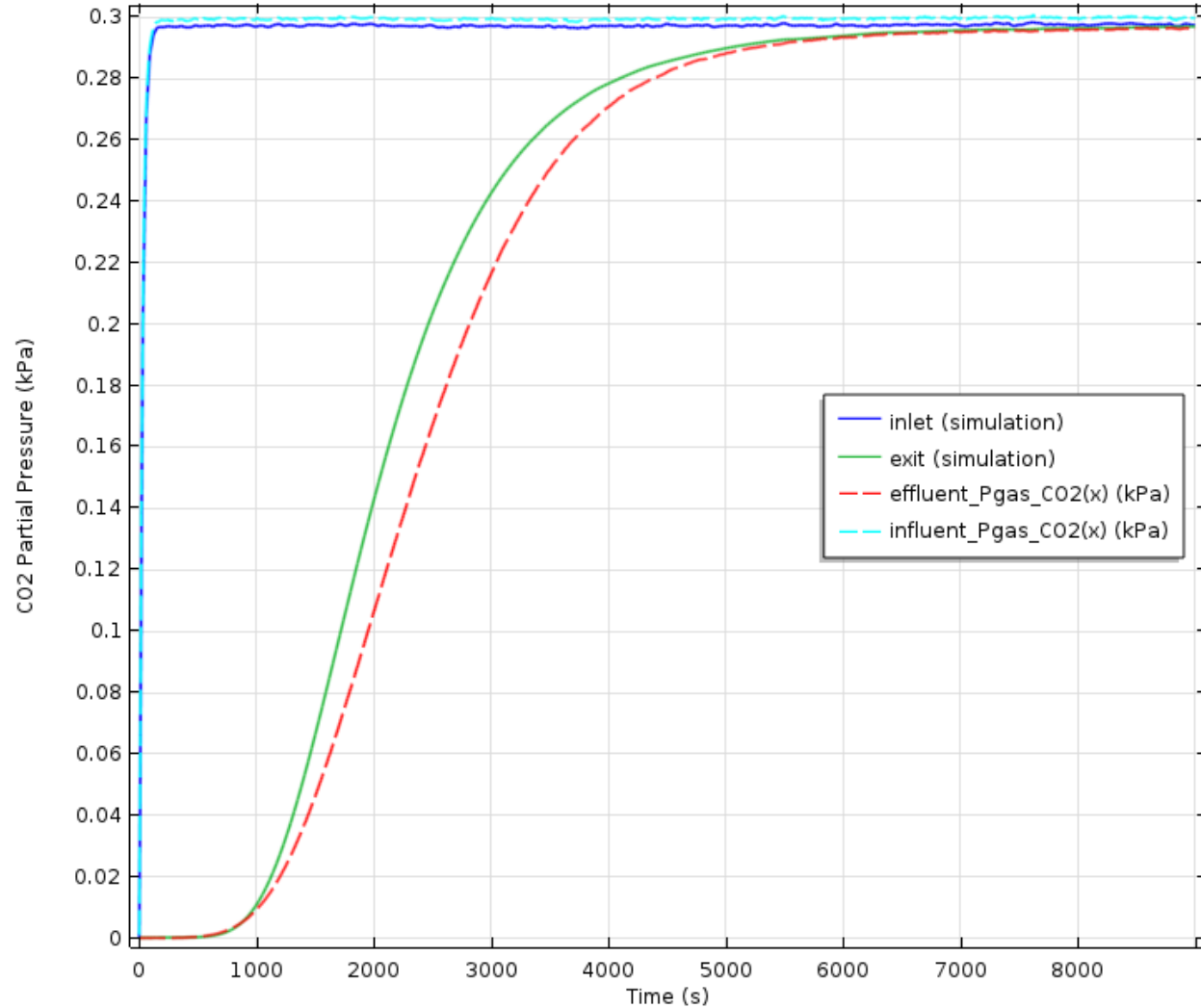
### 2D Brinkman Velocity (No Slip)



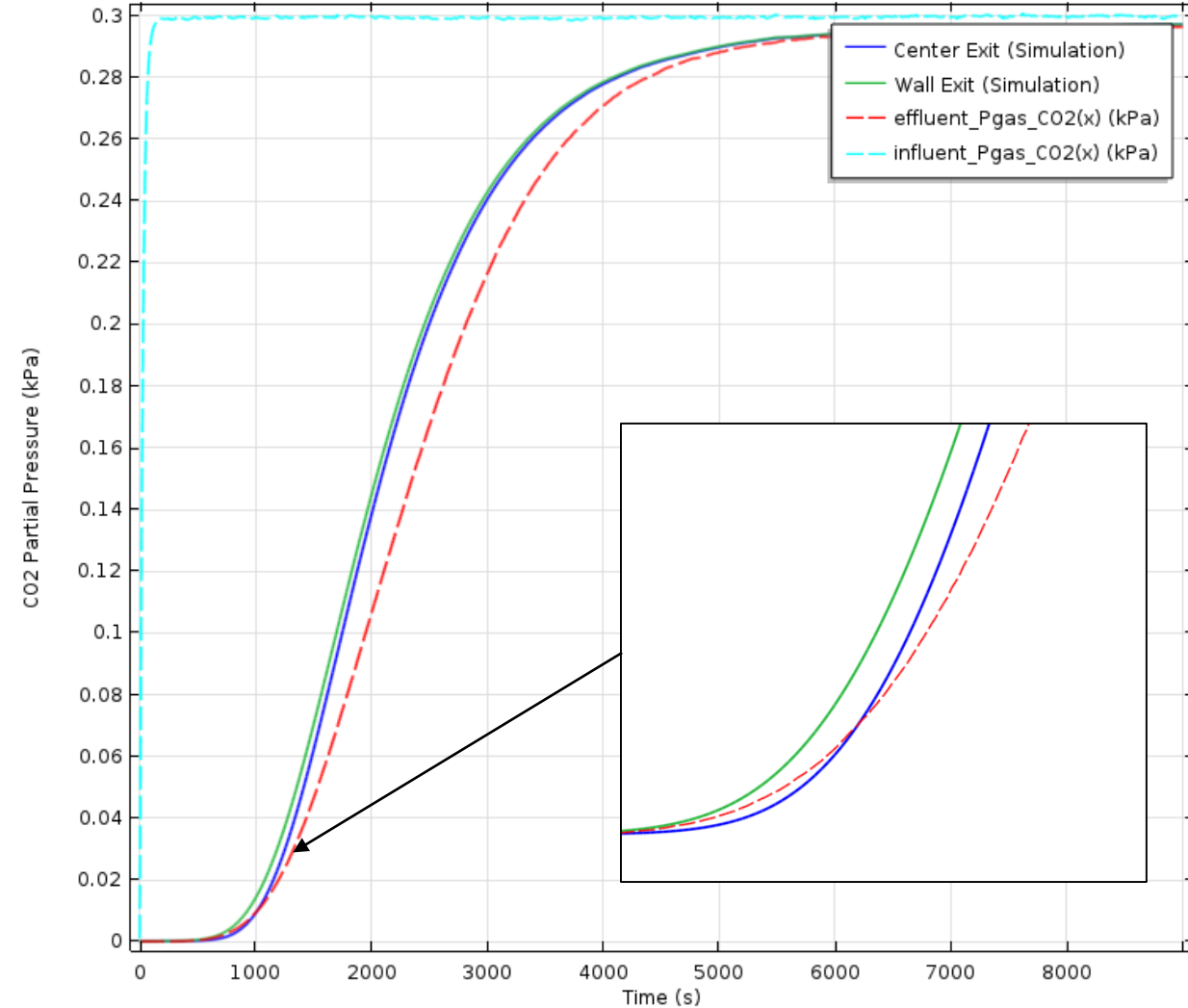
# Breakthrough Curve



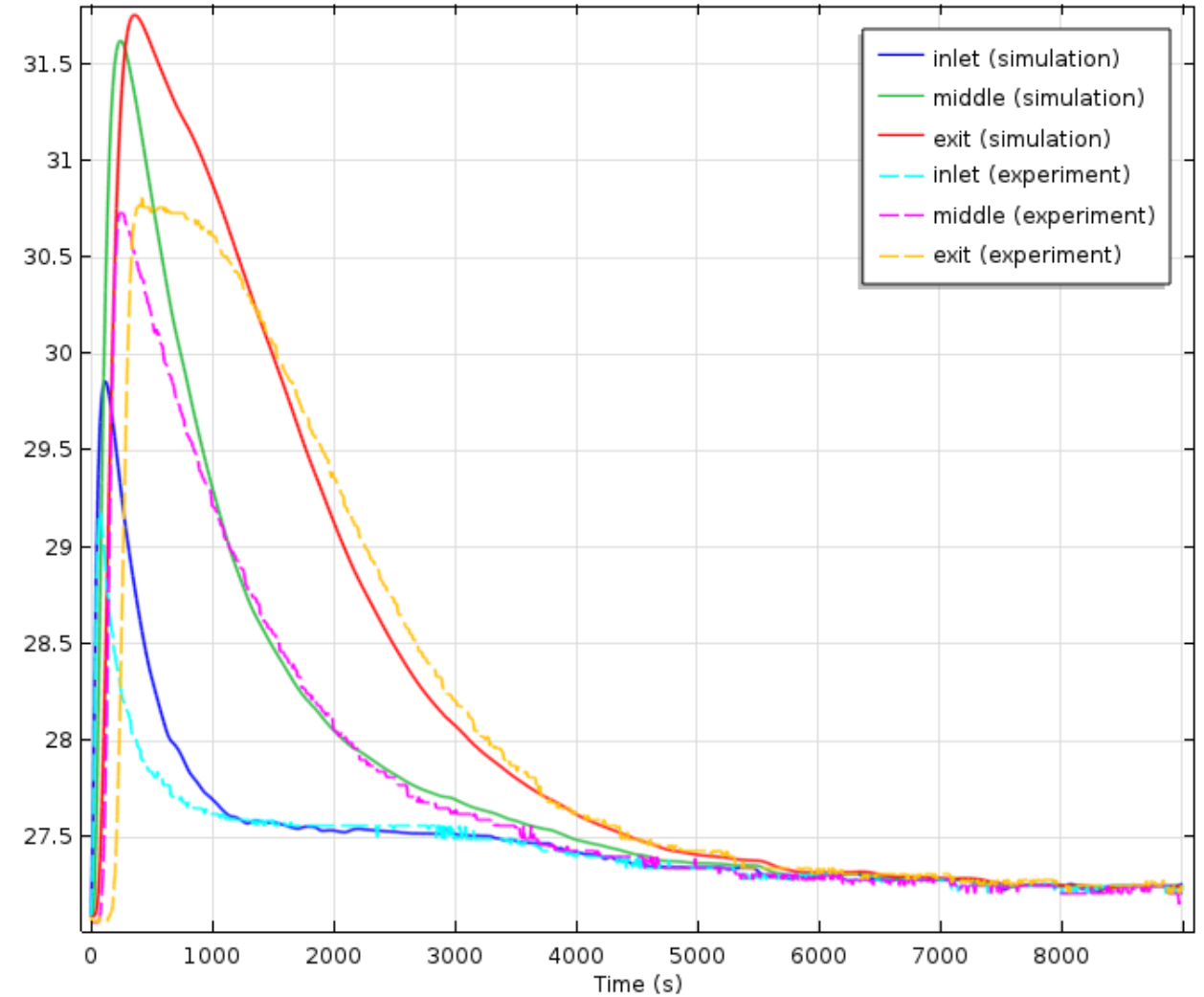
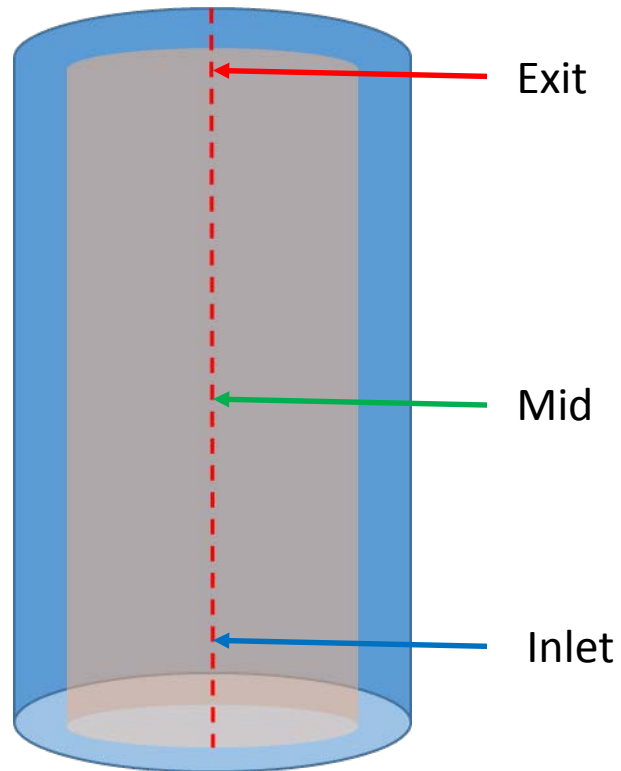
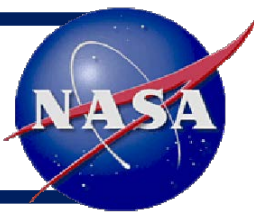
## 1D Darcy



## 2D Brinkman Velocity (No Slip)



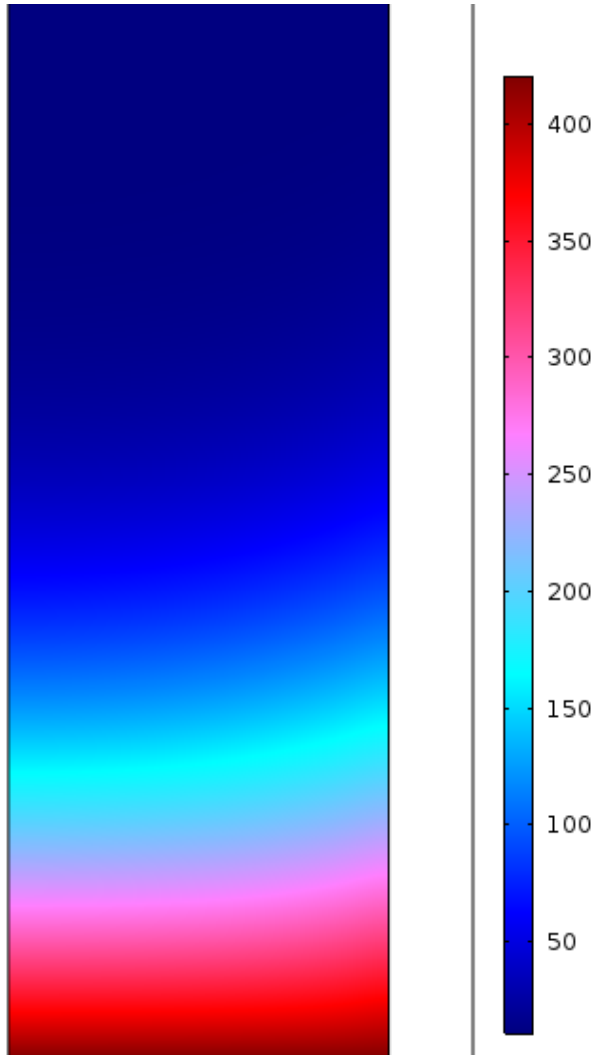
# Axial Temperature



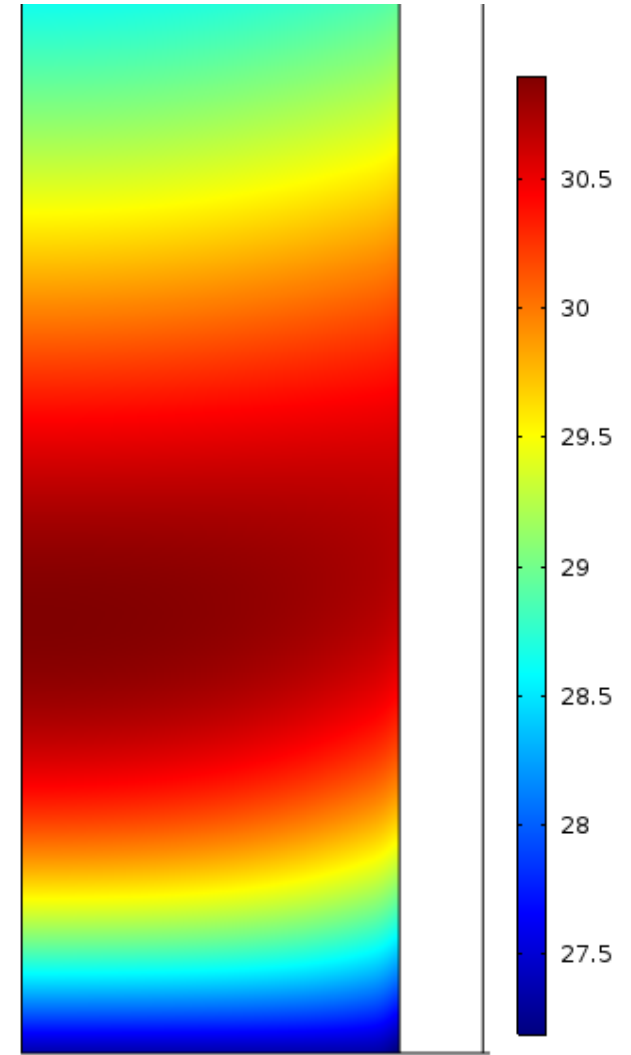
# Bed Loading and Temperature



Time=15 s CO<sub>2</sub> Bed Loading (mol/m<sup>3</sup>)



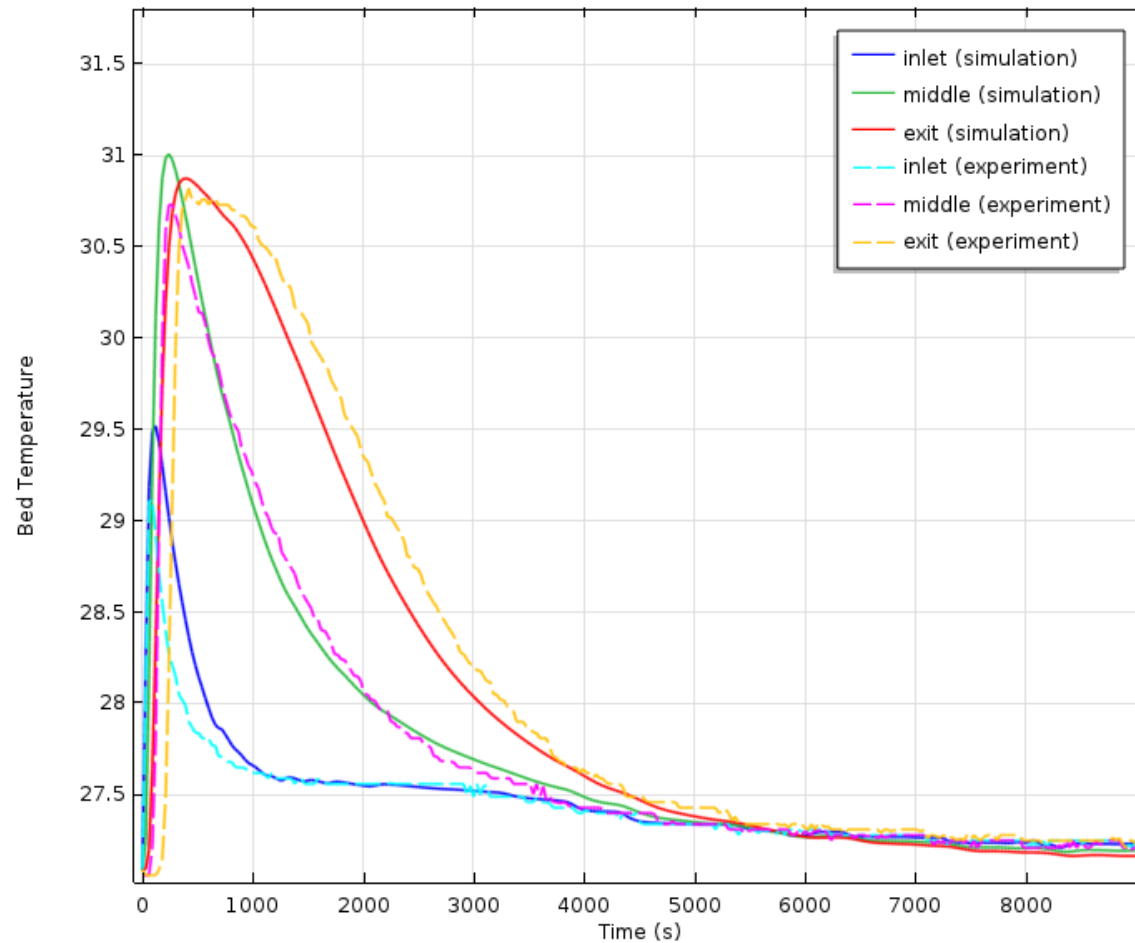
Time=15 s Surface: Temperature (degC)



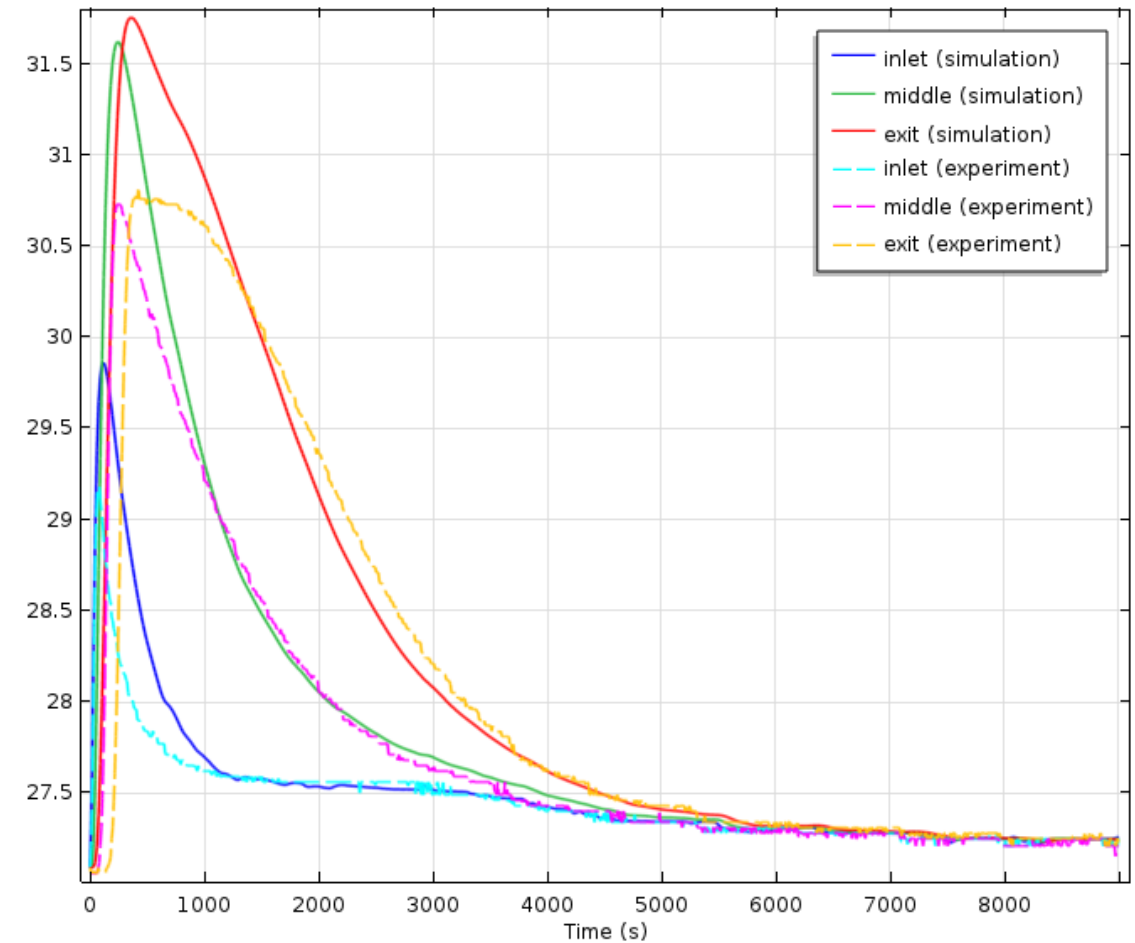
# Temperature Comparison



## 1D Darcy



## 2D Brinkman (No Slip)



# Conclusion/Future Work



- It's the first step in understanding how to model channeling at the wall with a no slip condition
- Learn and modify assumptions to improve correlations
- Upgrade to Free and Porous Media
- Vacuum Characterization test has been modified with vacuum instrumentation. Post processes desorption data
- Compare COMSOL desorption model to VC test data